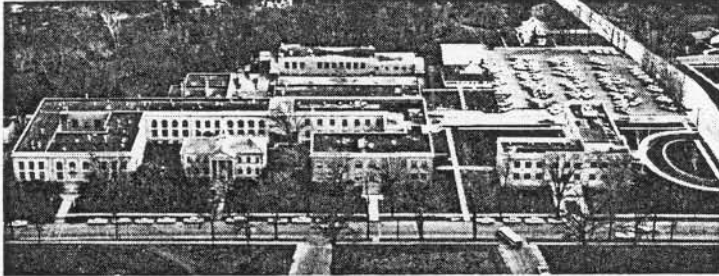


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**REACTIONS OF HYDROGEN WITH ALKALI CARBONATE/SULFATE SMELT**

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# REACTIONS OF HYDROGEN WITH ALKALI CARBONATE/SULFATE SMELT

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## ABSTRACT

This paper describes the reactions of hydrogen with alkali carbonate-sulfate-sulfide smelts. These reactions were studied by contacting sodium sulfate-sulfide-carbonate melts with a purge containing various mixtures of hydrogen, water vapor, and carbon dioxide in nitrogen. The results of this study help to determine the importance of the  $H_2$  reactions within the kraft furnace.

The reactions of  $H_2$  with a  $Na_2CO_3$ - $Na_2SO_4$  melt were found to generate both  $Na_2S$  and  $NaOH$  and to be dependent on the gas-melt interfacial area. These reactions occur in the interfacial melt film with  $H_2$  never achieving equilibrium with the melt. Initially, both the reduction of  $Na_2CO_3$  to form  $NaOH$  and the reduction of  $Na_2SO_4$  to form  $Na_2S$  are very rapid with 80% of the  $H_2$  supplied to the melt consumed. Once a few percent of  $NaOH$  is formed, the reduction of  $Na_2CO_3$  becomes quite slow.

Hydrogen reduction of  $Na_2SO_4$  was found to be an autocatalytic reaction with the autocatalytic behavior due to the formation of  $Na_2S$ . It was found to be nearly first order in  $H_2$  partial pressure and to have an activation energy of 22,000 cal/mol.

## INTRODUCTION

Hydrogen may occur in the kraft furnace from either black liquor pyrolysis or from the reaction of  $CO$  with  $H_2O$ . Borg, *et al.* (1) reported  $H_2$  concentrations of 3% directly above the bed. Hydrogen may either react with the  $Na_2SO_4$  to form  $Na_2S$  and  $H_2O$ , or it may react with  $Na_2CO_3$  to form  $NaOH$  and  $CO$ . The objective of this project is to identify the  $H_2$  reactions that will occur within the kraft furnace, and to determine the rate controlling process and significance of these reactions. Two products of these reactions,  $Na_2S$  and  $NaOH$ , are important to the operation of the kraft furnace. The first,  $Na_2S$ , is the desired form of sulfur, and the second,  $NaOH$ , has been implicated in corrosion problems within the furnace. Through increased knowledge of how these compounds are formed, it may be possible to control their formation within the furnace.

## PREVIOUS RESEARCH

Little quantitative information is available on the reactions of  $H_2$  with alkali carbonate-sulfate melts. Atomic International (2) conducted the most extensive research on these reactions. In this research,  $H_2$  reduction of sulfate was studied by bubbling hydrogen through an alkali carbonate-sulfate melt contained in a graphite crucible. The reaction was followed by periodically sampling the melt and analyzing it for sulfide. The melts used

for this study consisted of sodium-potassium-lithium carbonates, which form low-temperature melting systems and which enabled the reaction to be studied over a temperature range of 600 to 840°C. It was believed that at these temperatures the sole reaction that would occur was hydrogen reduction of sulfate. Although carbon dioxide was not normally collected during these experiments, it was sampled during a few experiments and was detected at levels indicating hydrogen reduction of carbonate was also occurring. At these temperatures the reaction was slow, with most reduction experiments requiring 14 to 40 hours. Water was collected during the experiments but was not used to follow the reaction rate.

Hydrogen reduction of sulfate was found to be an autocatalytic reaction with the rate increasing as the sulfide content of the melt increased. The reaction was also catalyzed by iron and tin salts. The reaction was zero order in sulfate and was dependent on the  $H_2$  partial pressure to the 0.65 power at  $H_2$  pressures from 0.25 to 10 atm. Using limited temperature data, the iron catalyzed reaction was determined to have an activation energy of 28.0 kcal/mol. The reaction rate was dependent on the melt-gas interfacial surface area.

## EXPERIMENTAL SYSTEM

The reaction of hydrogen with the alkali carbonate-sulfate melts was studied by either bubbling  $H_2$  through the melts or introducing  $H_2$  above stirred melts and monitoring the  $H_2$ ,  $CO$ , and  $CO_2$  content of the off-gas. These experimental systems are illustrated in Fig. 1 and 2. The  $H_2$  and  $N_2$  were metered through the mass flow meters and entered the melt through a ceramic tube. The off-gas from the reactor passed through an adsorbate water trap to a  $CO_2$ - $CO$  analyzer. From this analyzer the gases passed through a  $CO_2$  trap before entering an  $H_2$  analyzer.

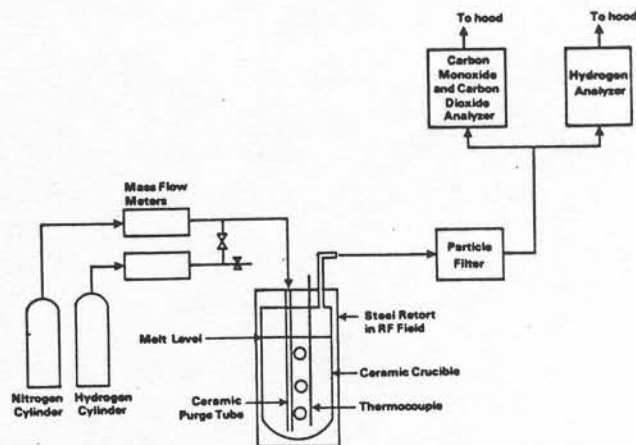


Figure 1. Experimental system with gases introduced below melt's surface.

These experimental systems allowed the effects of the temperature, melt composition, gas composition, and gas flow rate on the reactions to be studied. One deficiency of the system with the purge introduced below the melt's surface is that it does not